

Density, Porosity, and Heat Capacity Characteristics of Ash Deposits from a 1.5 MW Coal Furnace

Oxyfuel Technologies I

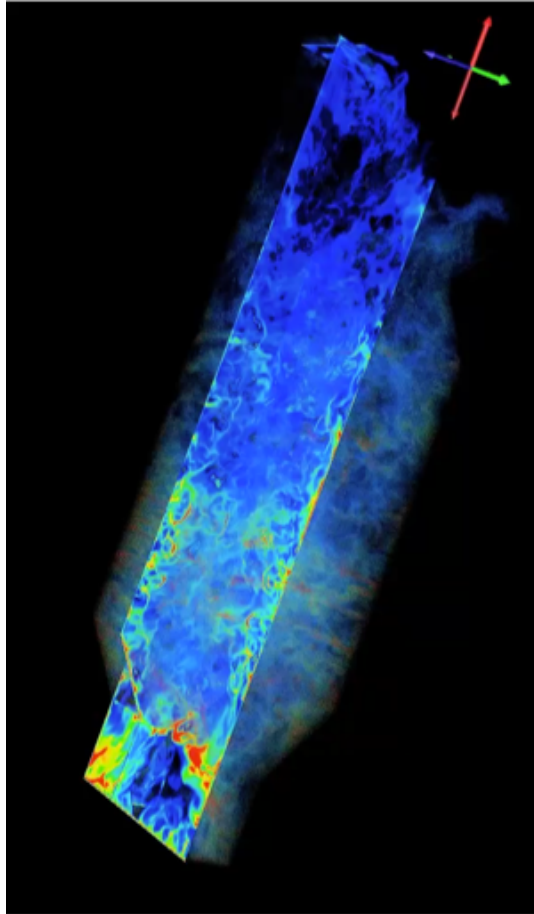
The 41st International Technical Conference on Clean Coal & Fuel Systems

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Department of Chemical Engineering, University of Utah

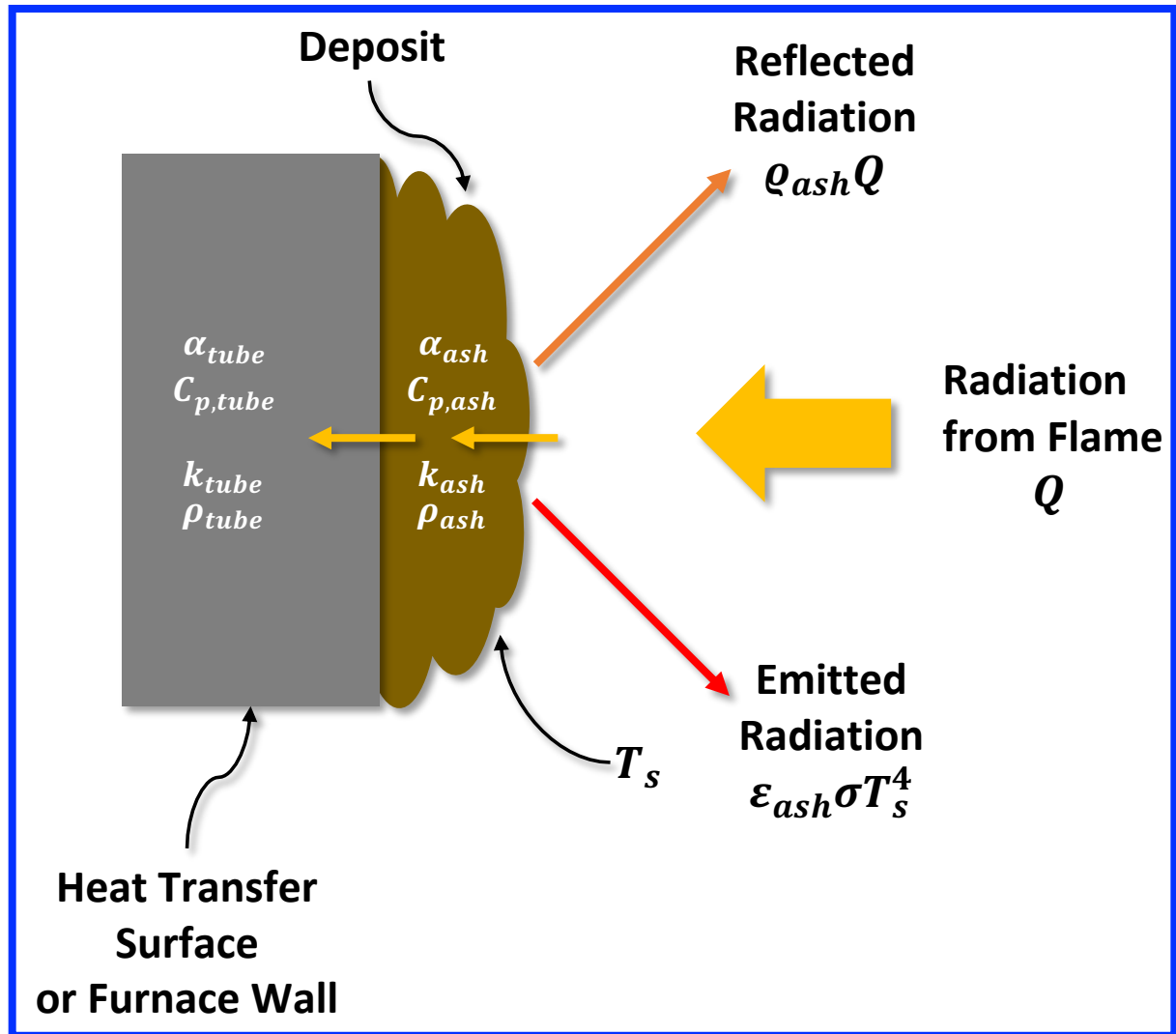


Introduction

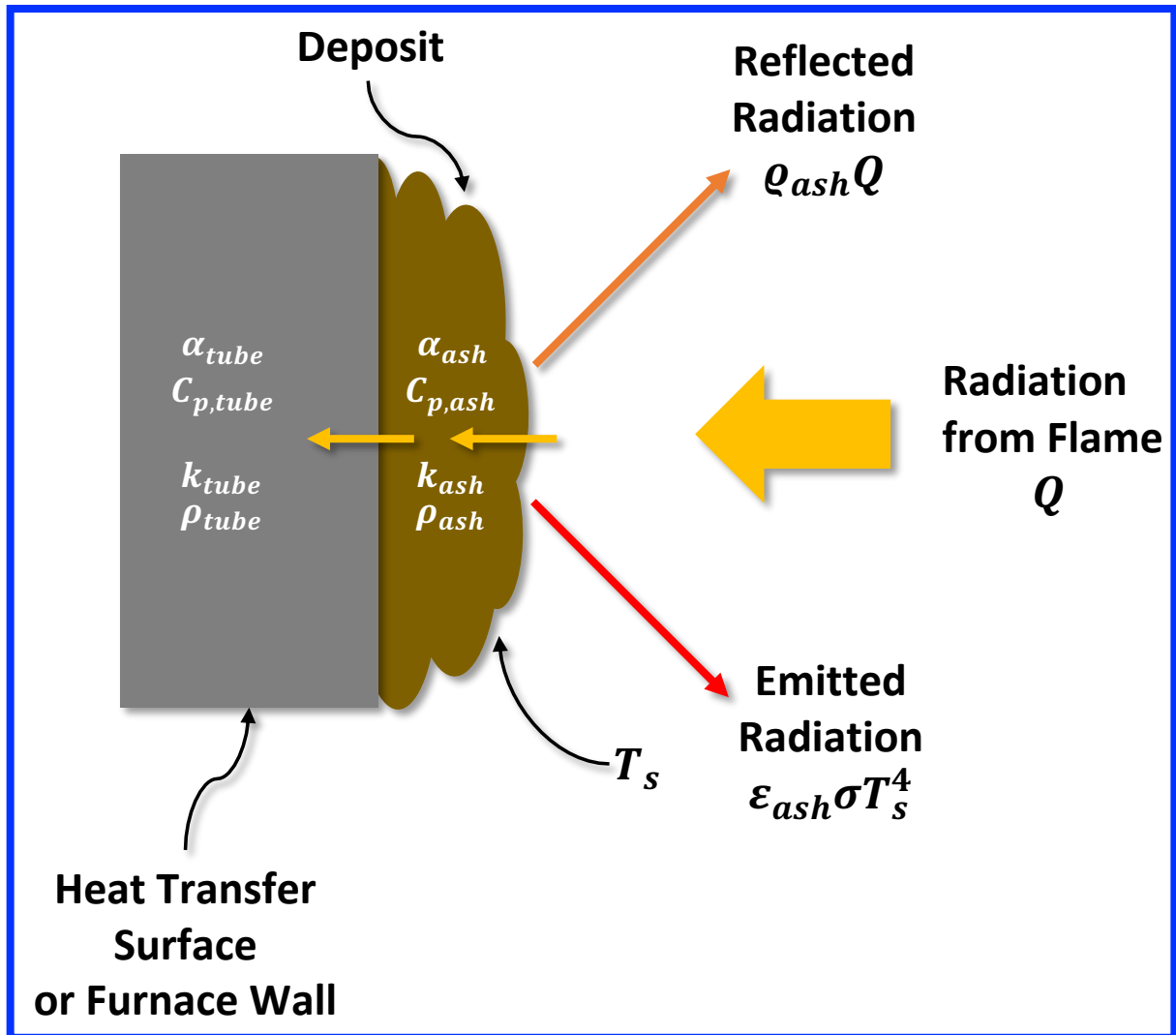


- Carbon-Capture Multidisciplinary Simulation Center
- Simulations of oxy-coal boilers
- Model uncertainty reduced and characterized through **experimental** validation and verification/uncertainty quantification (V&V/UQ)
- Vary, compare, and contrast experiment and analysis techniques to capture uncertainty and error

Heat Transfer

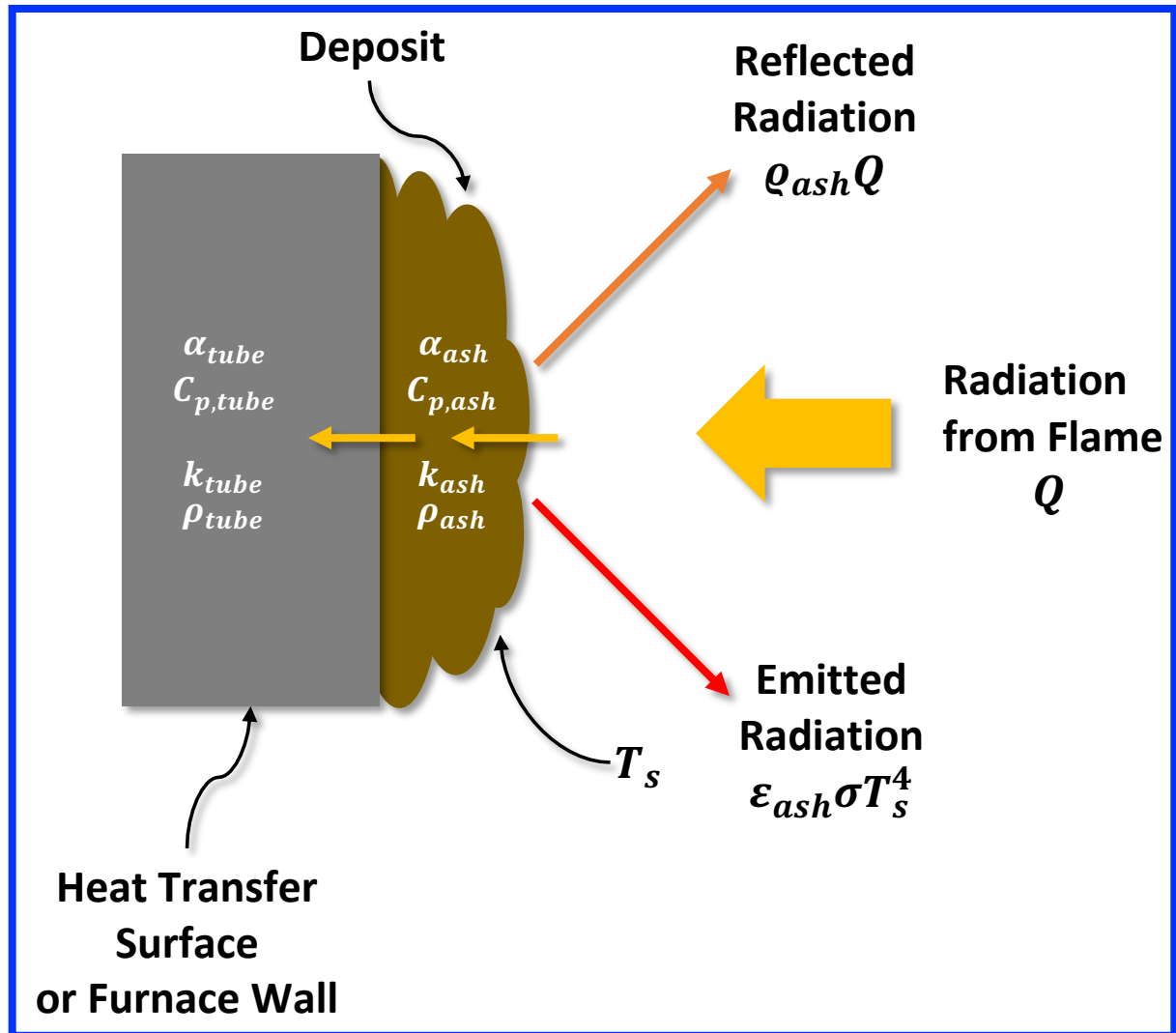


Heat Transfer



ρ = reflectivity
 ϵ = emissivity
 k = thermal conductivity
 α = thermal diffusivity
 ρ = density
 C_p = heat capacity

Heat Transfer

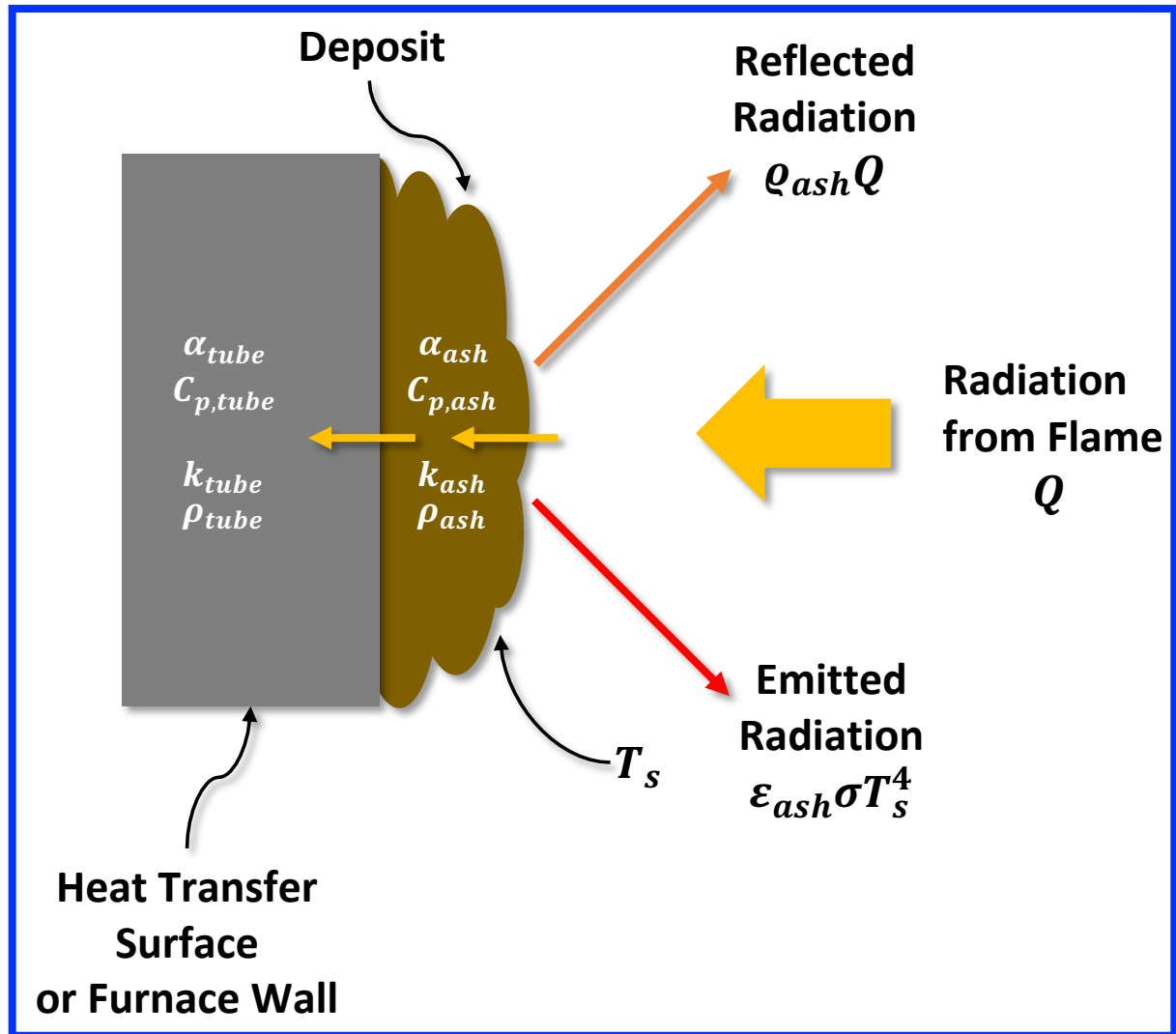


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Tube/Wall

Characterized at
high temperature

Heat Transfer



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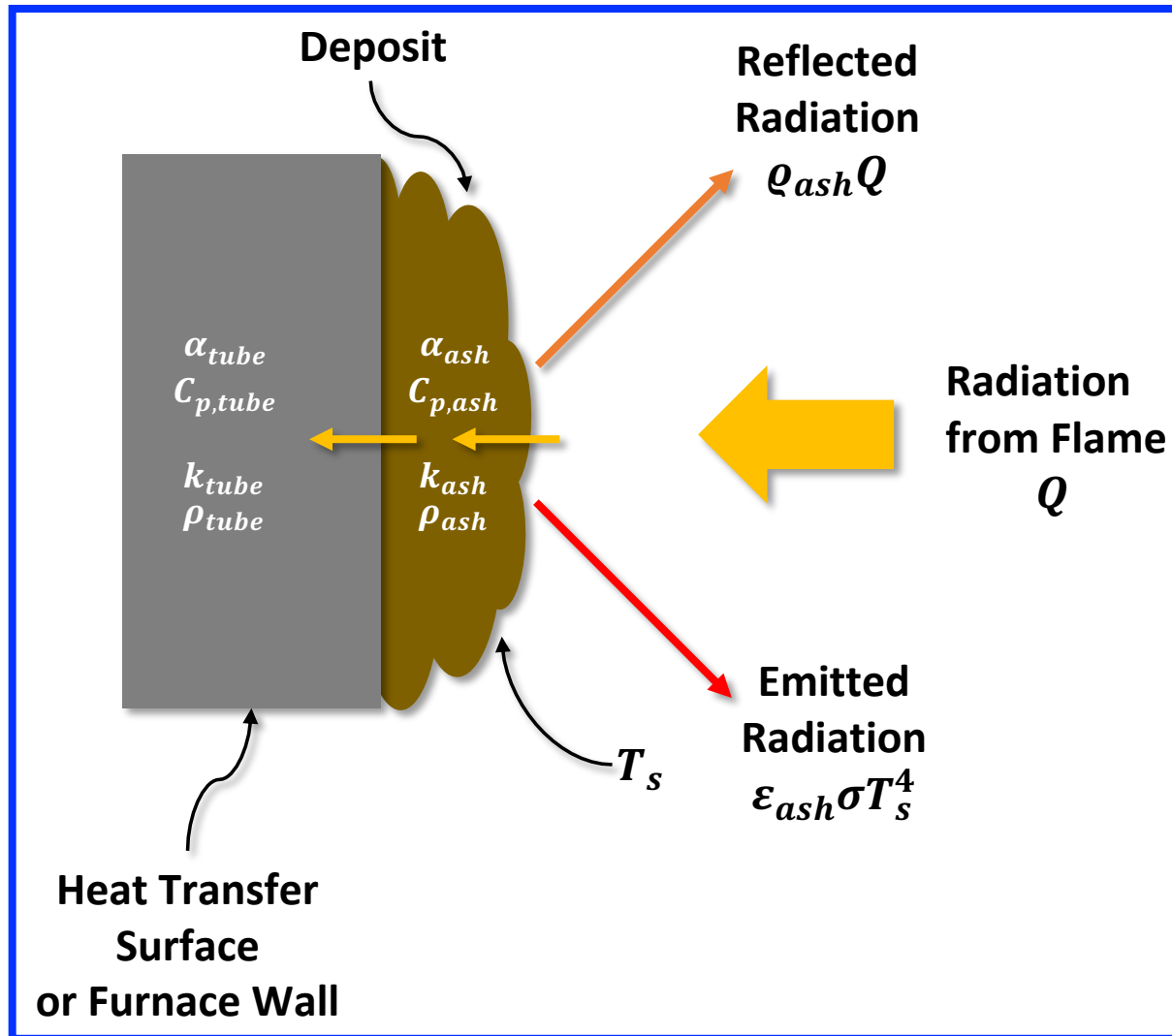
Tube/Wall

Ash/Slag

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?

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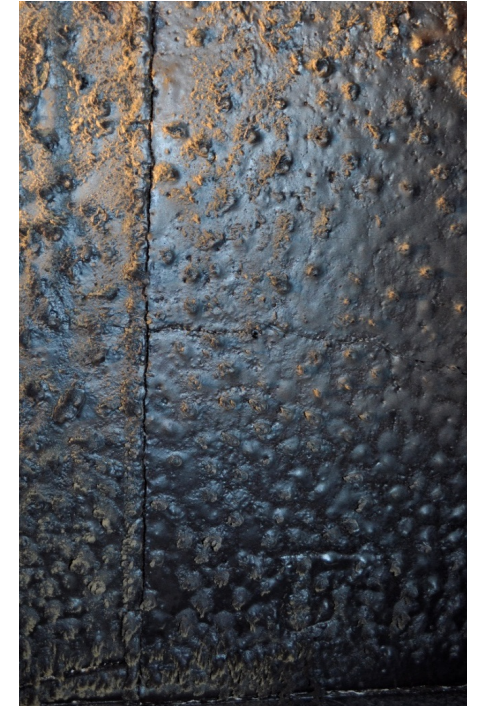
Ash/Slag

Characterized at high temperature

?

Deposits

- Highly variable
- Emissivity
 - Previous study with room temperature FTIR
- Thermal Conductivity
 - $\alpha = \frac{k}{\rho C_p}$
 - $k = \rho \alpha C_p$
 - Temperature dependence

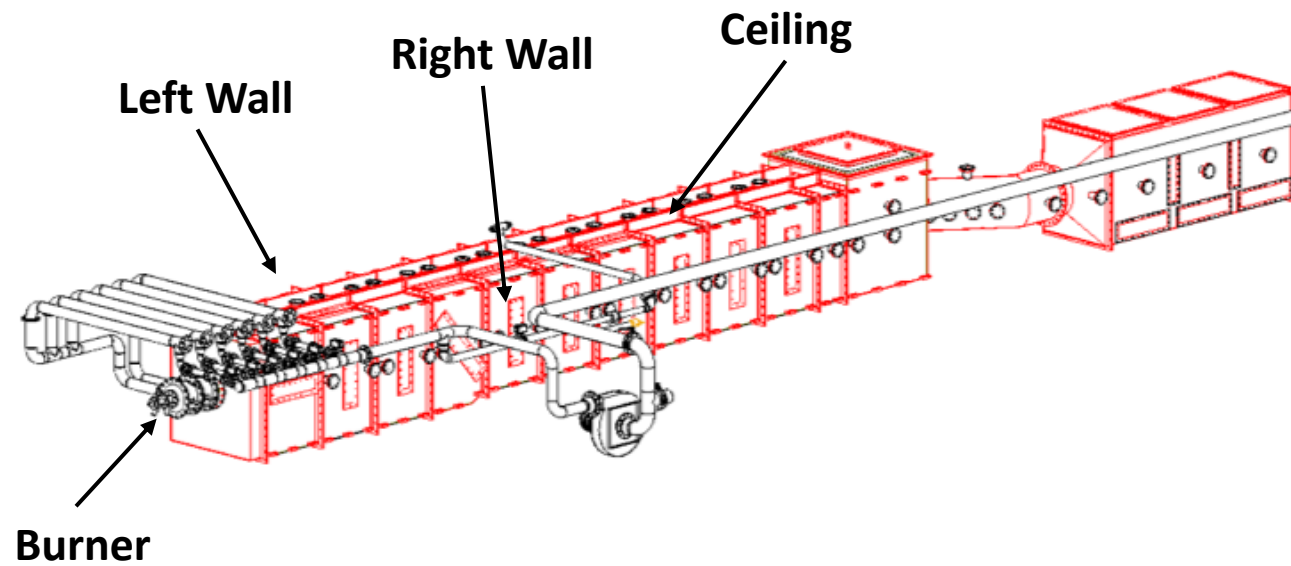


Experimental Design

- Industrial Combustion And Gasification Research Facility
- L-1500 Multifuel Furnace
 - 1.1m by 1.1m internal cross-section
 - 13.1m in length
- February 2015 oxy-coal campaign
 - Utah Sufco coal
 - Firing rate ~1.0 MW (3.5 MBtu/hr)
 - Coal feed rate: ~135 kg/hr (297 lb/hr)
 - Avg. excess oxygen ~3%
 - Exhaust CO₂ ~86-88%
 - Surface temperature (ceiling): ~1052 °C (1925 °F)

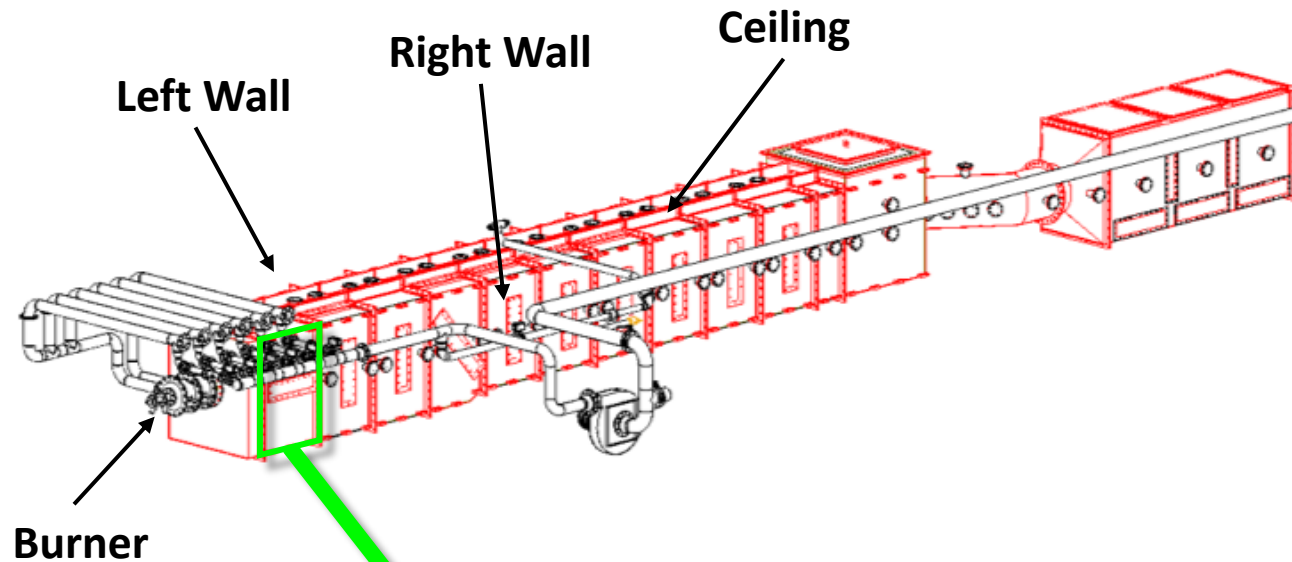


Experimental Design



- ~400 total sampling sights throughout the furnace in a 1 ft x 1 ft grid
 - Surfaces: left wall, ceiling, & right wall

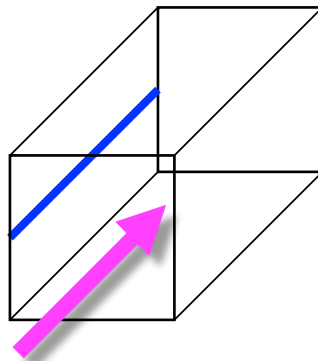
Experimental Design



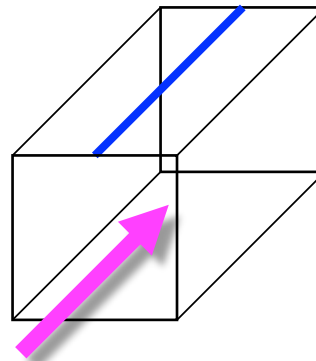
- ~400 total sampling sights throughout the furnace in a 1 ft x 1 ft grid
 - Surfaces: left wall, ceiling, & right wall
- Twelve sampling sights chosen for a preliminary study
 - Location: midline of each surface
 - Depth: 1, 2, 3, and 4 feet from burner on each surface
 - Highly radiative section of the furnace

 = sampling location
 = flame

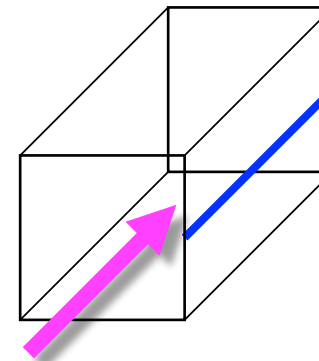
Left Wall



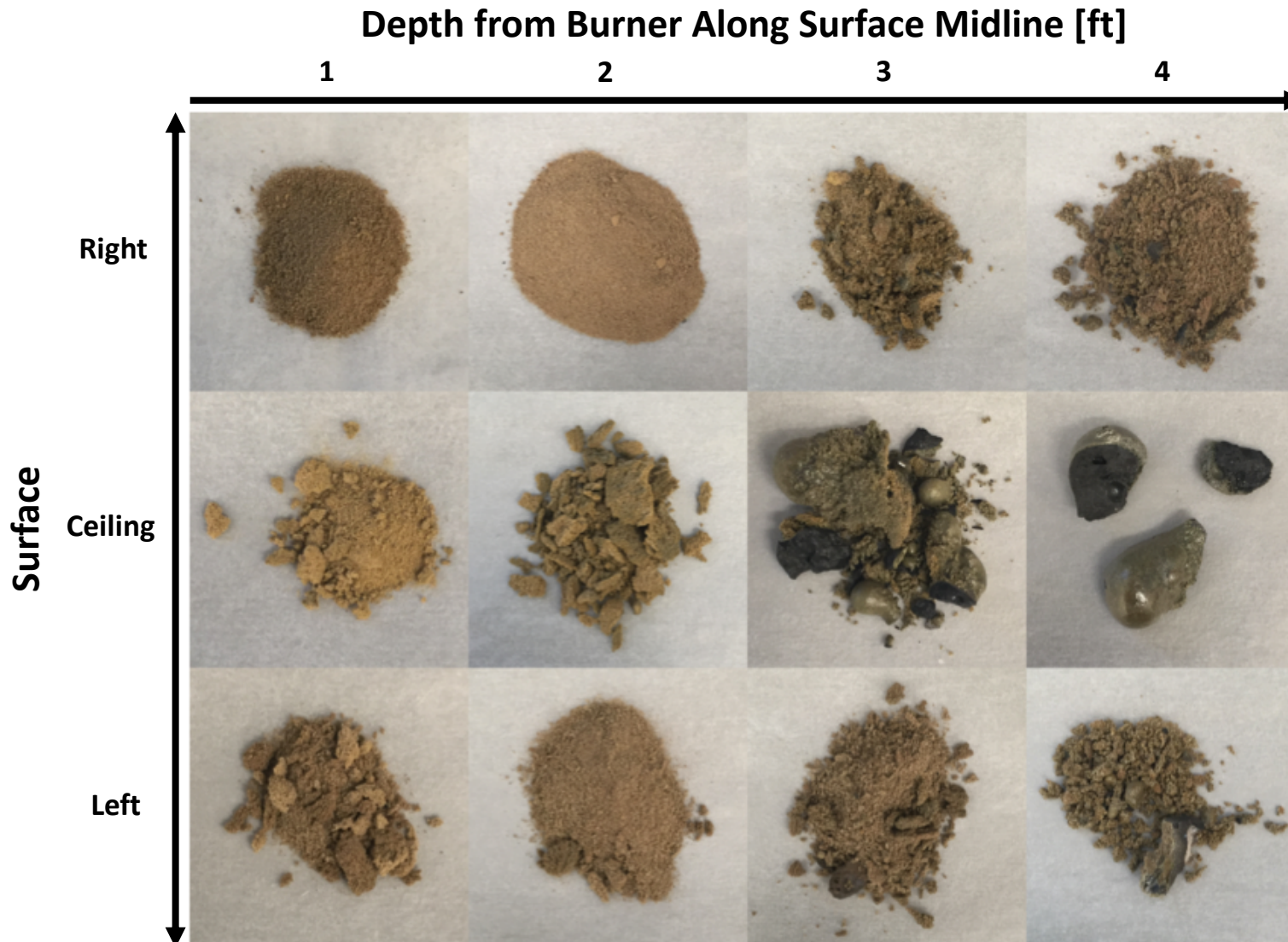
Ceiling



Right Wall

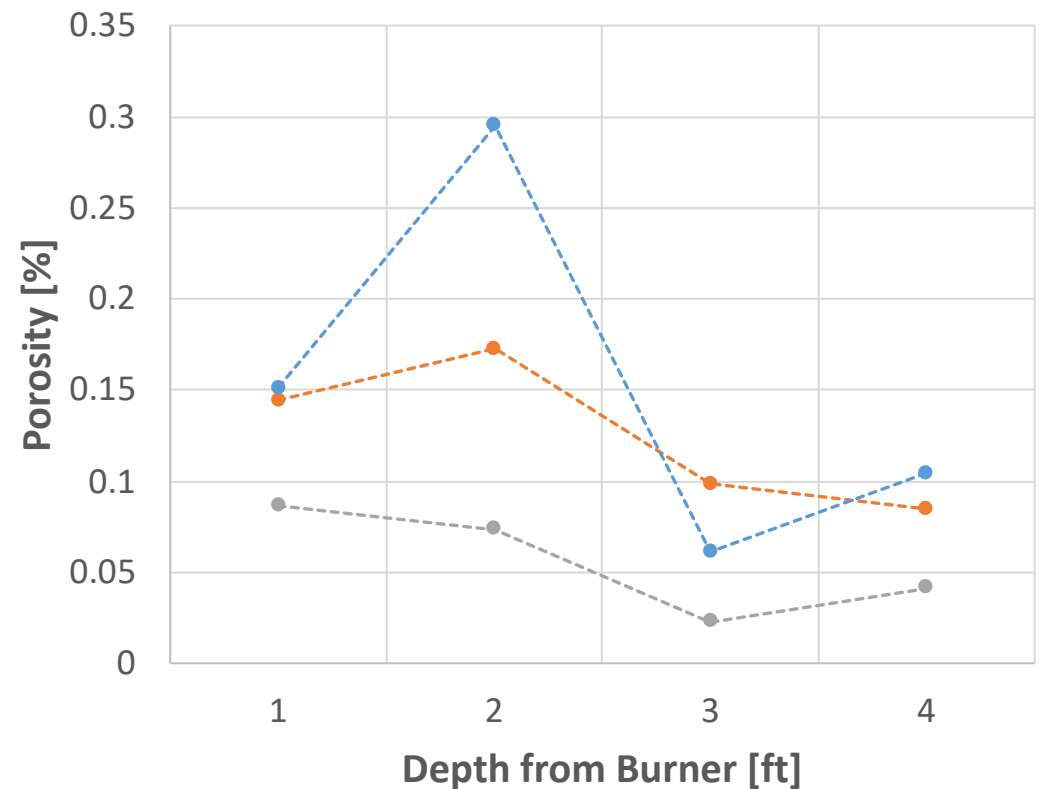
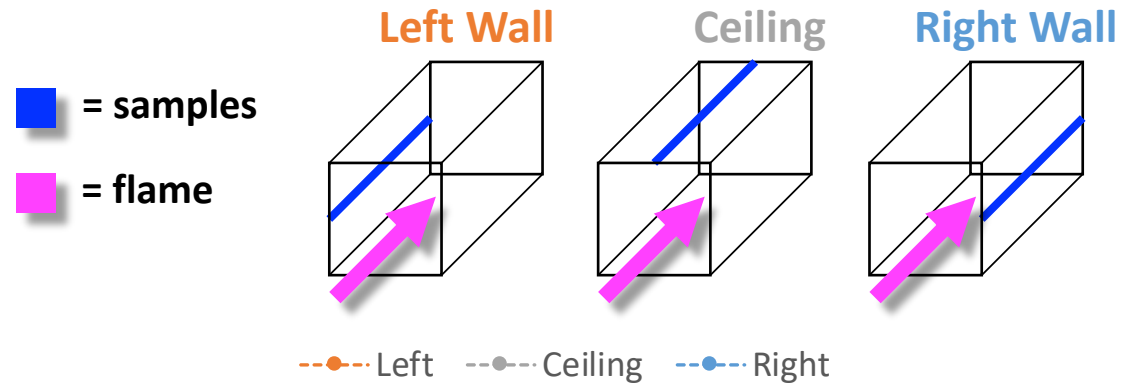


Samples



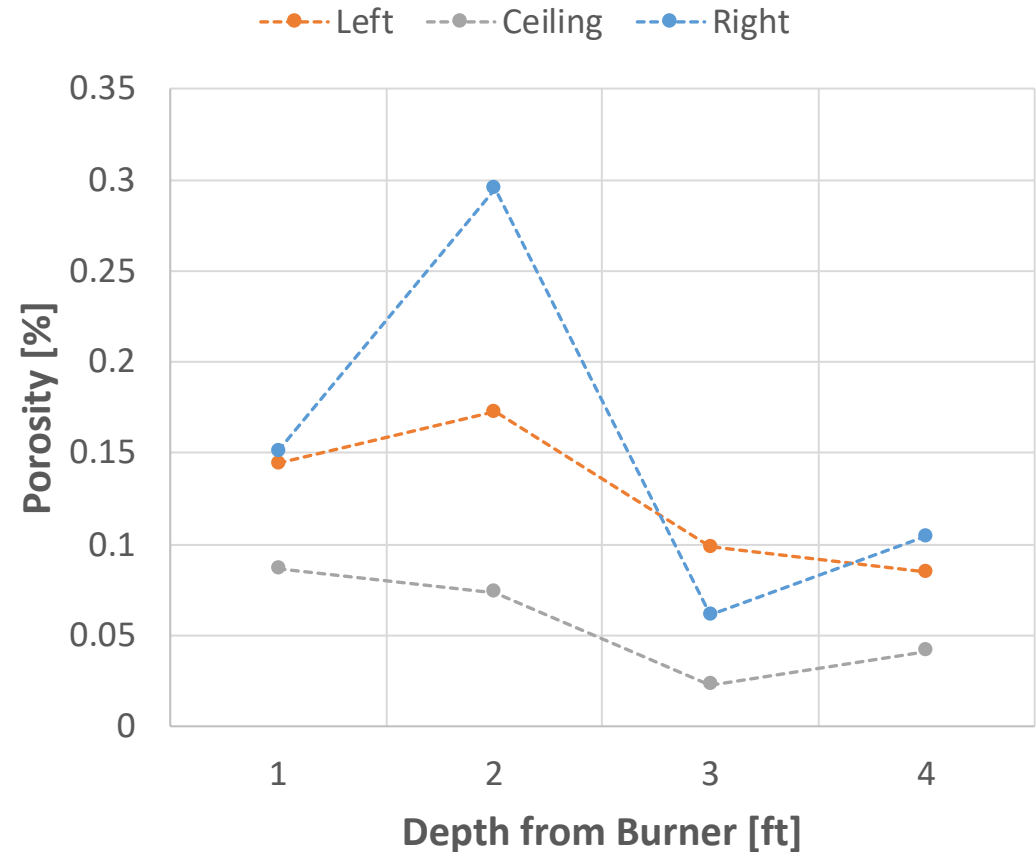
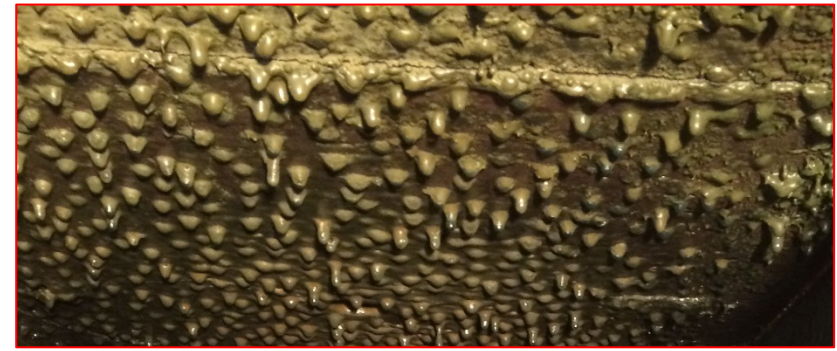
Porosity

- Porosity
- $\phi = \frac{V_{pores}}{V_{solid} + V_{pores}} \times 100\%$
- Total pore volume
 - BET analysis
- Total solid volume
 - Pycnometry
- Very low for all three surfaces
- Porosity does not appear to be a strong function of depth for the first four feet of the furnace
- Slightly higher in the left and right walls than in the ceiling



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- Slightly higher in the left and right walls than in the ceiling
 - Ceiling deposits molten during operation



Thermal Conductivity - Method

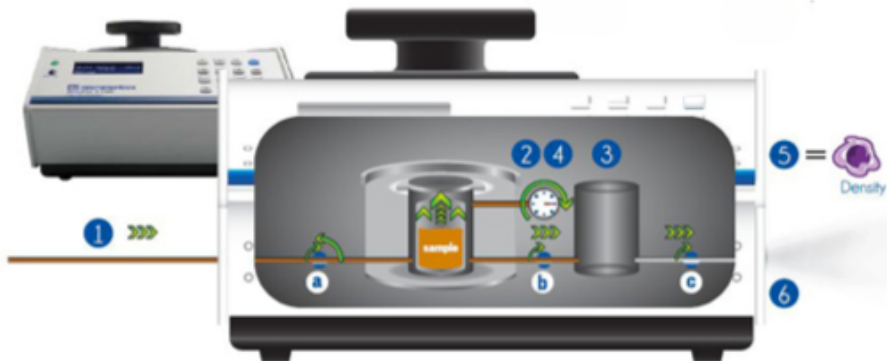
- Measurements of α , ρ , and C_p for deposit samples
- Higher temperature regimes when available (α , C_p)

$$k_{eff} = \rho_{meas} \alpha_{meas} C_p_{meas}$$

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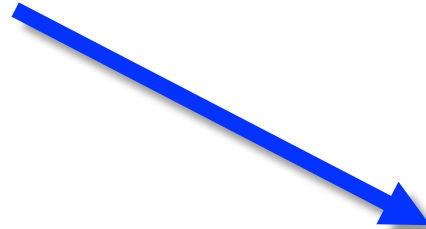


Automatic Helium Gas Pycnometry

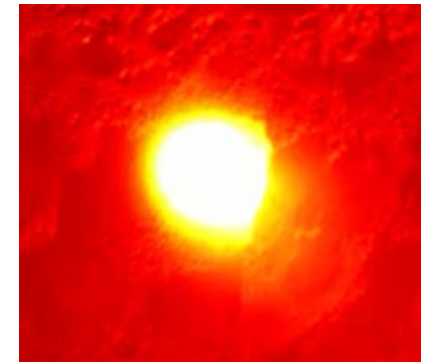
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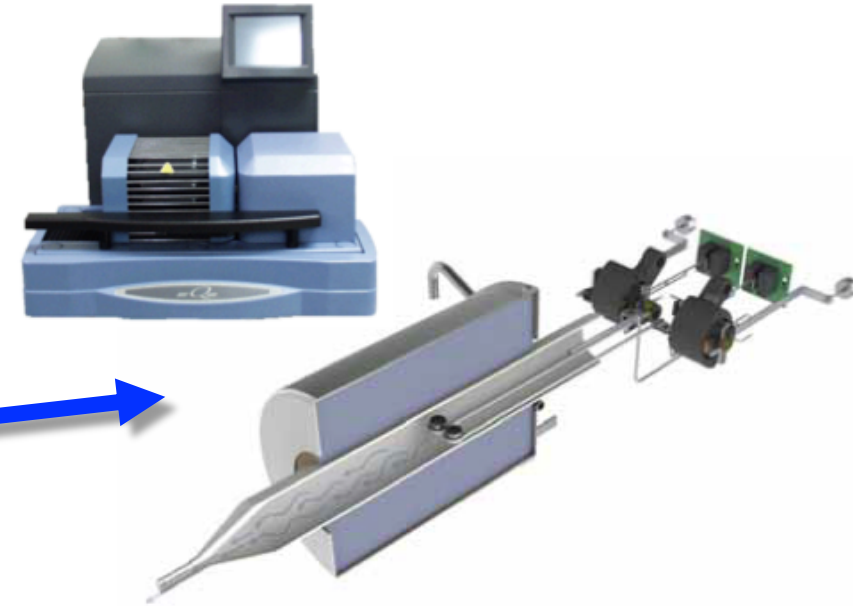


IR Camera Thermal Image Processing

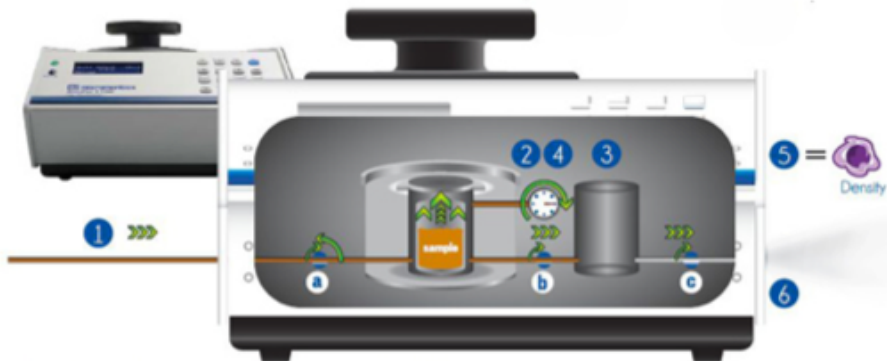
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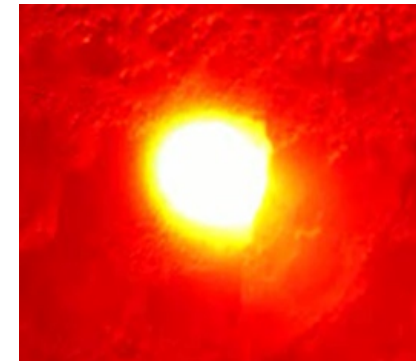
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Differential Scanning Calorimetry



Automatic Helium Gas Pycnometry

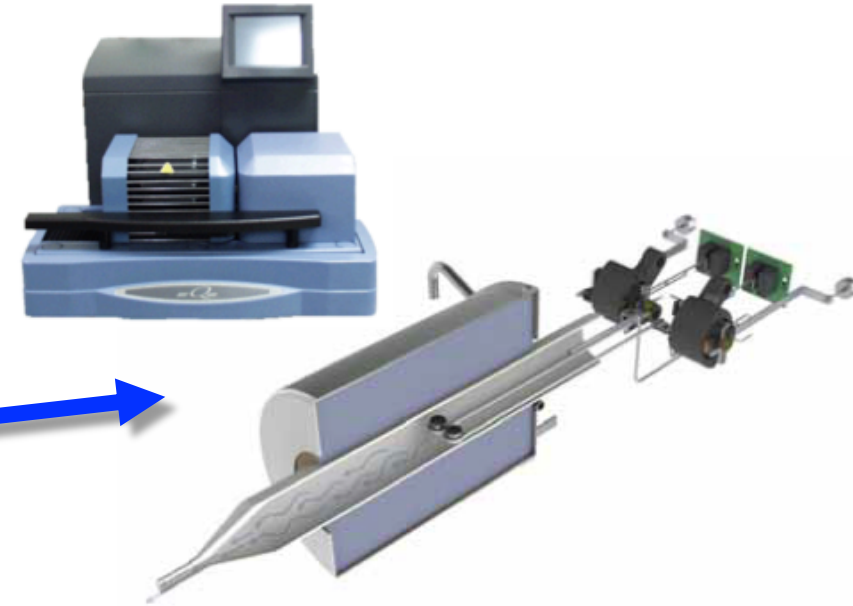


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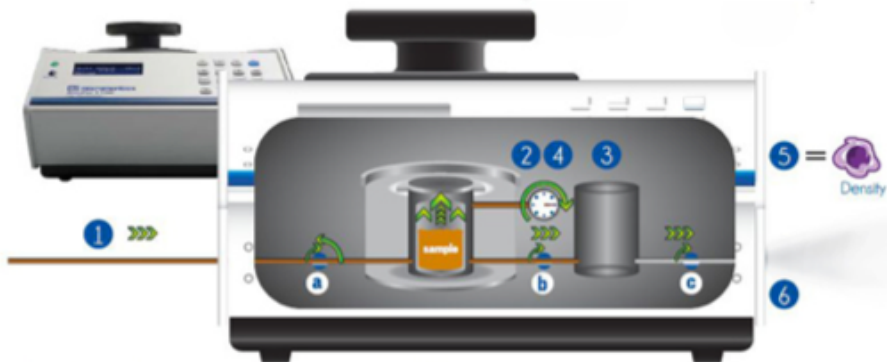
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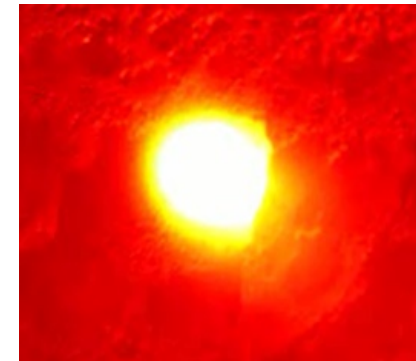
Differential Scanning Calorimetry



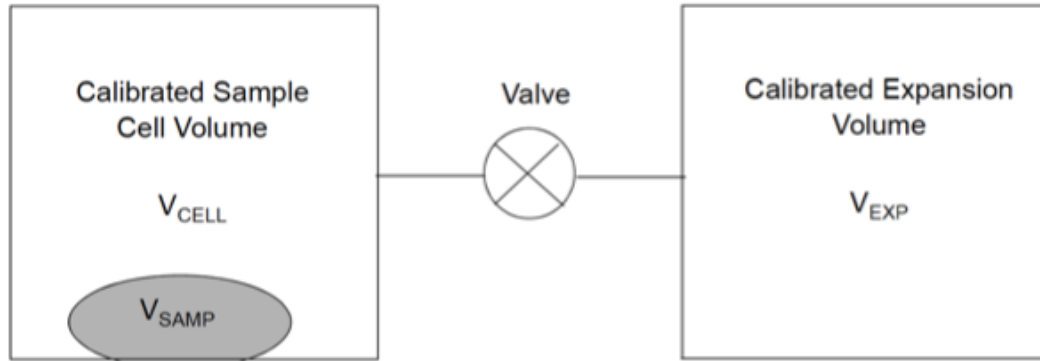
Automatic Helium Gas Pycnometry



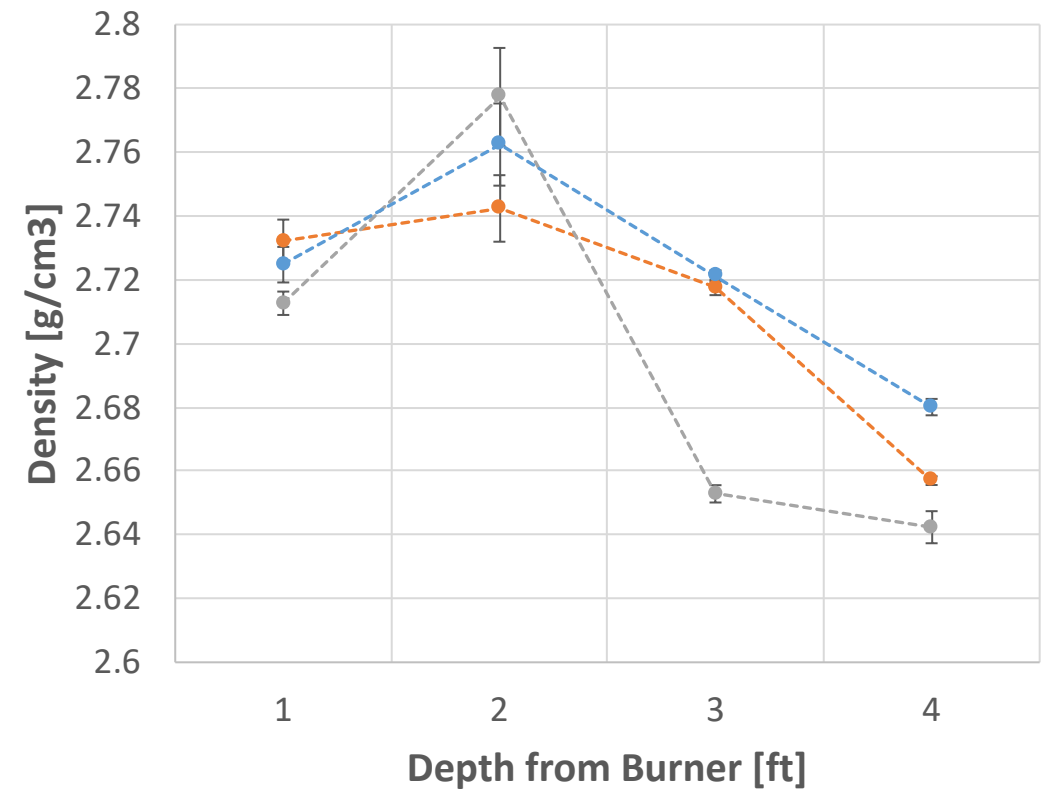
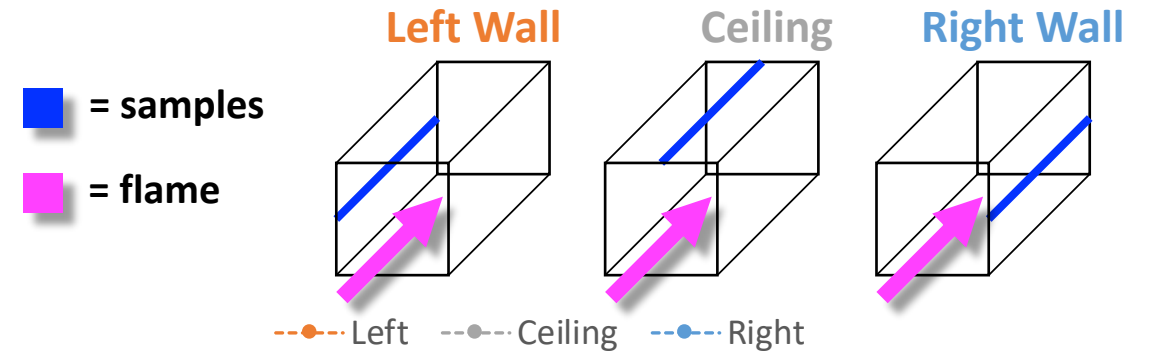
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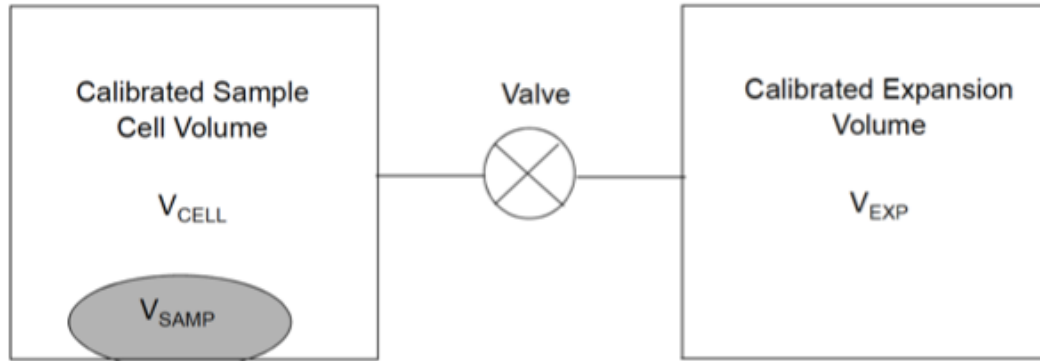
Solid Density



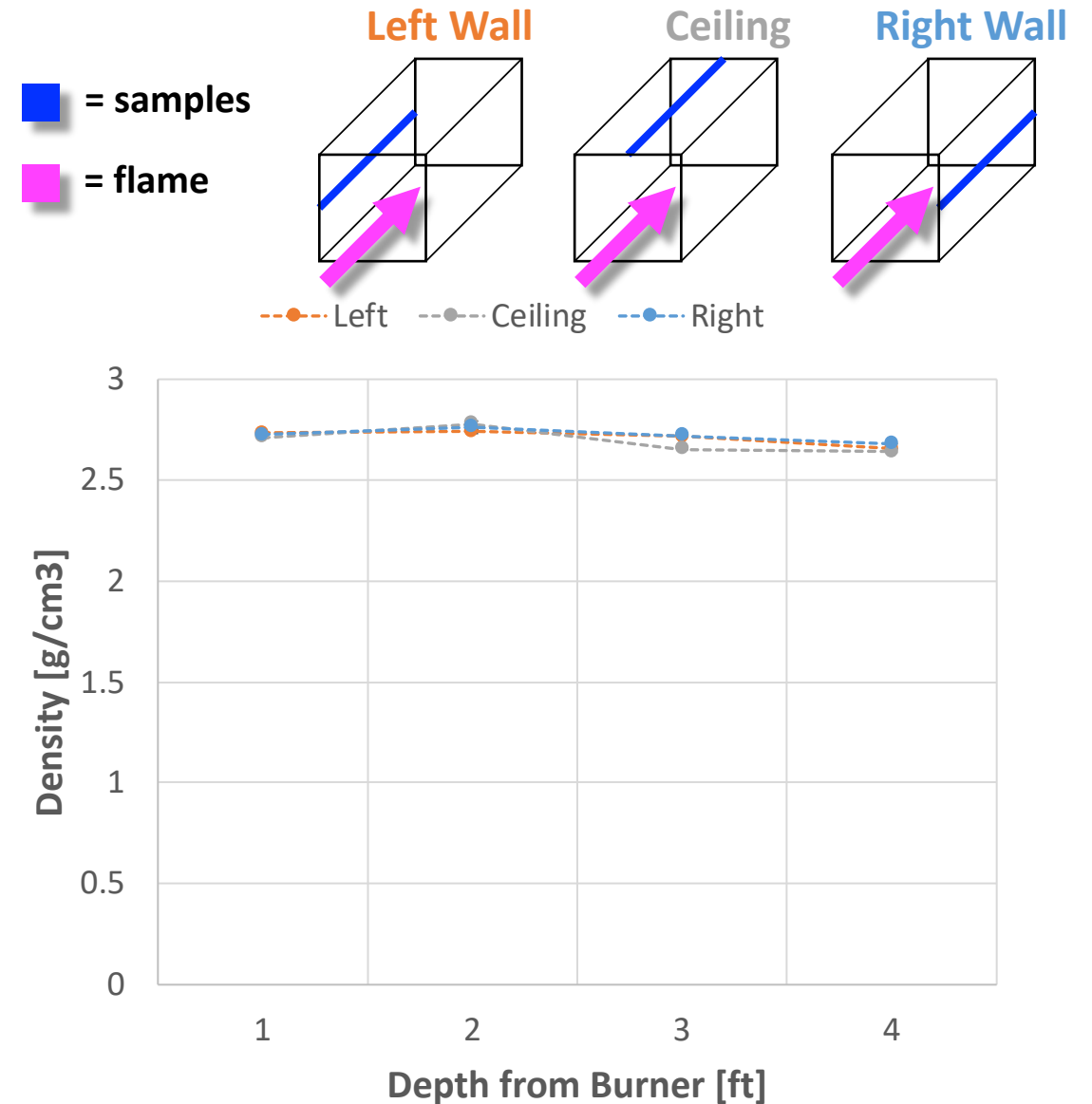
- Pycnometry
- $V_{samp} = V_{cell} - \frac{V_{exp}}{\frac{P_{1g}}{P_{2g}} - 1}$
- $\rho = \frac{m}{V}$
- Direct measurement of true (skeletal) density of samples
- Three replicates to capture instrument run error
 - 2 x Std. Dev.



Solid Density

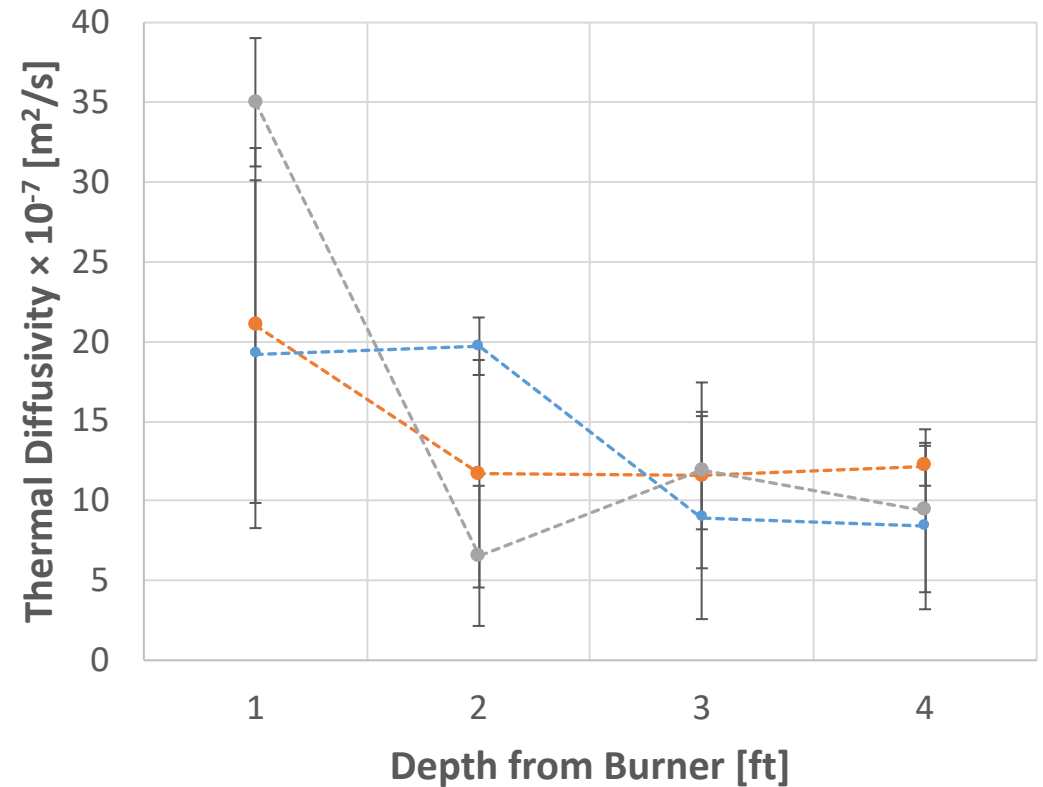
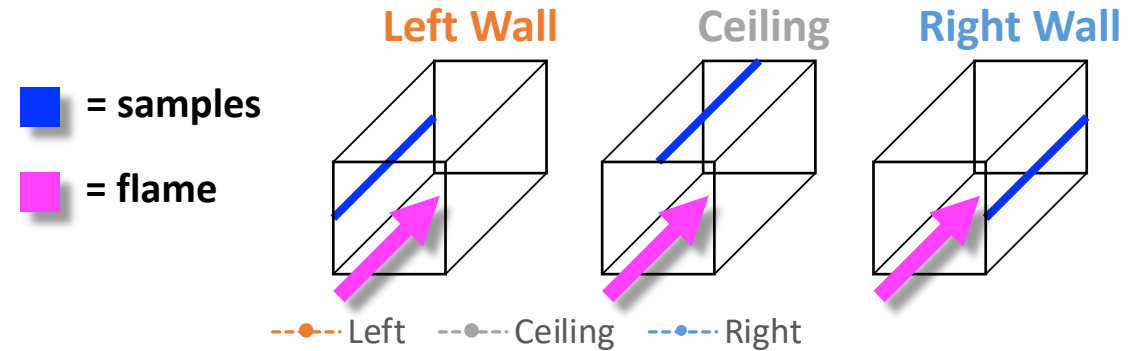


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- Three replicates to capture instrument run error
 - 2 x Std. Dev.
- Density does not appear to be a strong function of depth for the first four feet of the furnace



Thermal Diffusivity

- Thermal diffusivity determined in previous work using novel technique
- Surfaces covered in deposit were heated using an oxy-acetylene torch
- Infrared camera video was taken of the heated area
- Diminishing area of the heat was tracked with MATLAB using a threshold value
- Two-dimensional radius used to approximate hemispherical volume of dissipating heat
- The slope of the heat volume versus time was compared to a COMSOL simulation of pure refractory and related to yield the thermal diffusivity.
- Three replicates to capture measurement error
 - 1 x Std. Dev.
- Thermal diffusivity does not appear to be a function of depth for the first four feet of the furnace



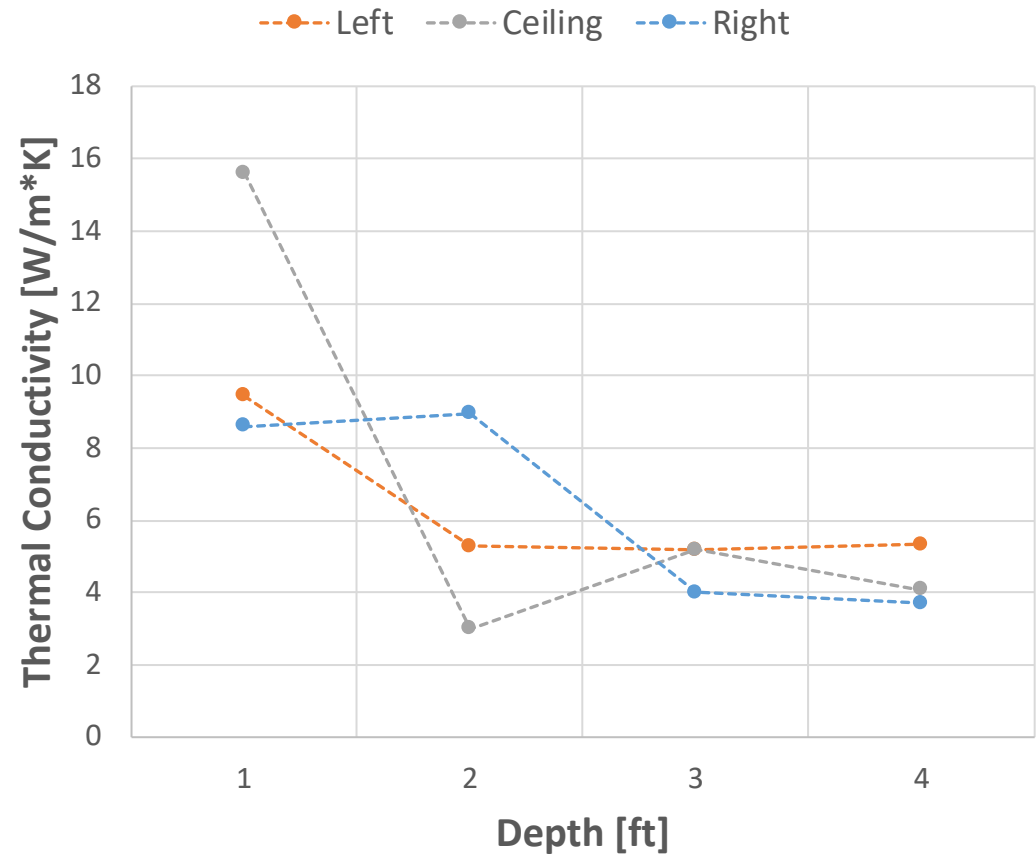
Heat Capacity

- Differential scanning calorimetry
- Direct measurement of heat flow
- Heat capacity calculated
 - $C_p = \frac{1}{m} \frac{(\delta Q/d\tau)}{(dT/d\tau)}$
- Data at 700 °C for ceiling sample at 1 ft depth – two runs
 - Low enough temperature to avoid molten state and glass transition
- High standard deviation

	Heat Capacity [J/kg*K]
Run 1	1404
Run 2	1884
Average	1644
Std. Dev.	340
2 x Std. Dev.	680

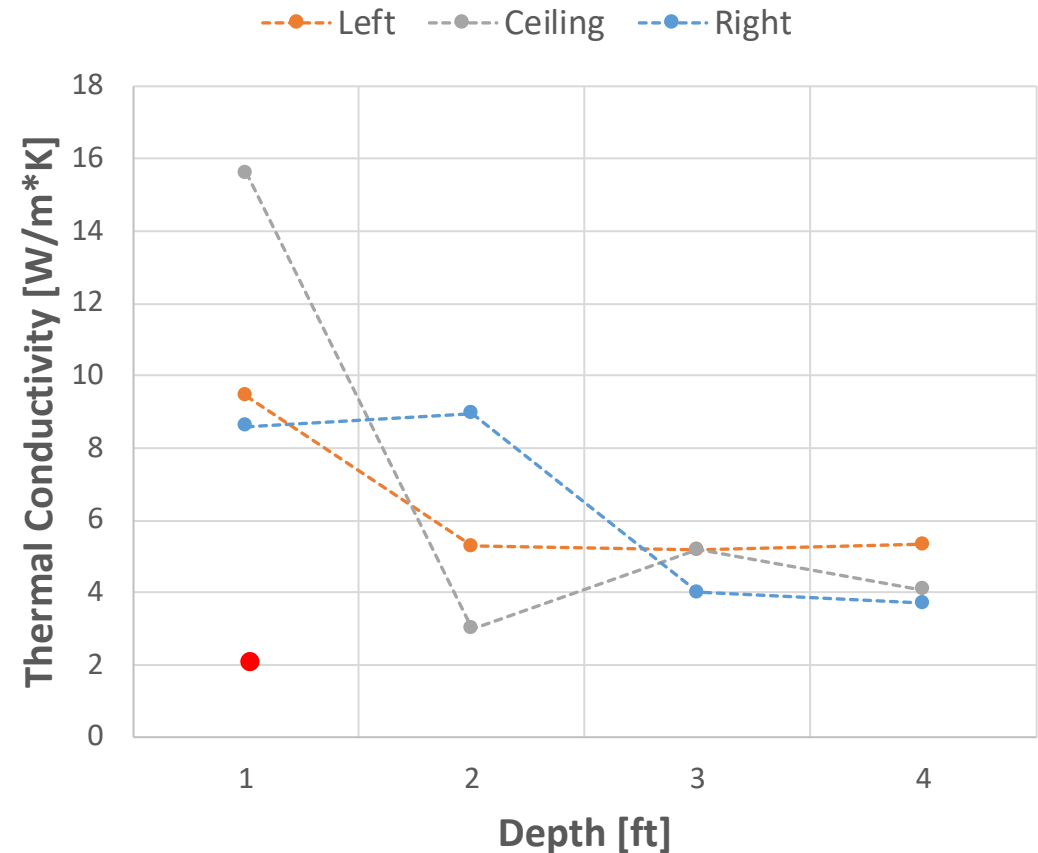
Thermal Conductivity - Result

- $k_{eff} = \rho_{meas} \alpha_{meas} C_{p,meas}$
- *Approximated using C_p measurement from sample for ceiling at 1 ft depth for a temperature of 700 °C
- Thermal conductivity does not appear to be a strong function of distance in the first four feet of the furnace
- High thermal conductivity may be due to potential sintering of samples – indicated by very low porosity
- Uncertainty in thermal diffusivity measurements from new technique may contribute to high thermal conductivities



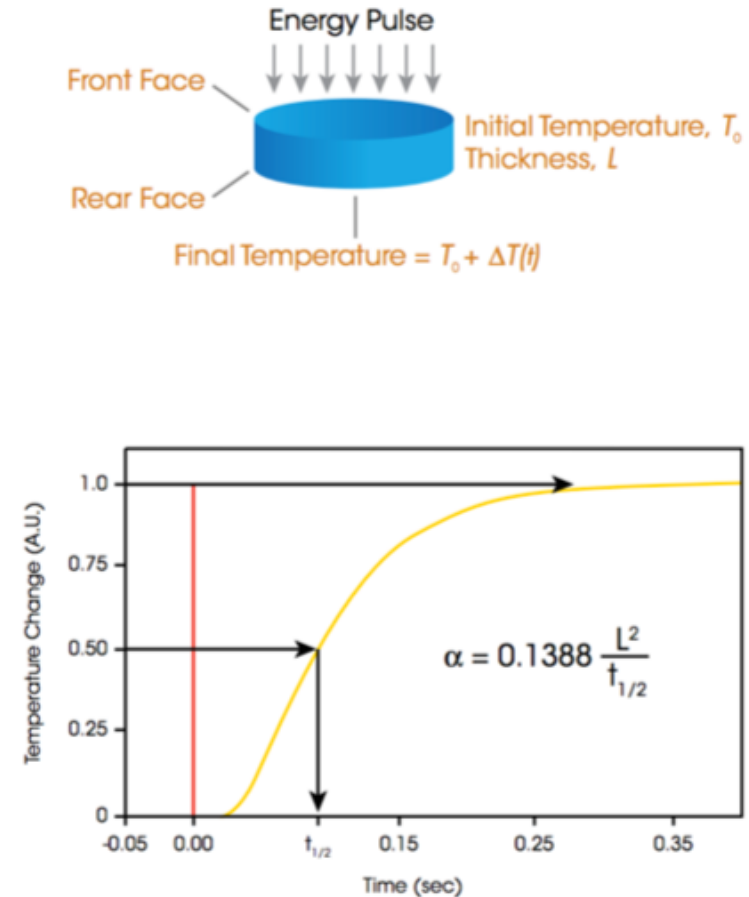
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 - Using a smaller literature value for α of $4.5 \times 10^{-7} \text{ [m}^2/\text{s]}$ gives $k_{eff} = 2.01 \text{ [W/m * K]}$ for the ceiling at 1 ft depth



Flash Method Validation

- Flash Measurement Technique
 - Measurements up to 2000 °C for validation of the presented approach to calculating effective thermal conductivity
 - Direct measurement of sample thermal diffusivity
 - Also produces heat capacity and thermal conductivity information



Summary

Conclusions

- Results for first four feet of L-1500 furnace
 - Low overall porosity
 - Samples may have sintered during furnace operation
 - Density does not strongly depend on depth
 - Low uncertainty in measurements due to low error
 - Thermal diffusivity does not seem to depend on depth
 - High uncertainty in measurements due to large error
 - Thermal conductivity is high for the oxy-coal deposits
 - May be due to potential sintering of samples
 - High uncertainty of thermal diffusivities from new technique
 - Thermal conductivity does not strongly depend on depth
 - High uncertainty in calculation due to approximation using only one sample heat capacity measurement at this time
- Overall, high temperature effective thermal conductivity has potential to be approximated by combining various property measurements
 - Will require further refinement in future work

Future Work

- Larger sample size
 - Farther from burner
 - Increase spread on surfaces
 - Up to 400 samples available
- High temperature density measurements
- Validation/verification of thermal diffusivity
 - Flash method
 - Refine technique to account for refractory contribution
- More detailed analysis of heat capacity
 - Higher temperatures with glass transition
- X-ray fluorescence and SEM to determine composition and structure
- High temperature FTIR
- Development of instrument models for the various measurement techniques to fully characterize sources of uncertainty

Instrument Figure References

Pycnometer figure (slides 17-20): <http://www.micromeritics.com/Product-Showcase/AccuPyc-II-1340.aspx>

IR camera figure (slides 18-20): <http://www.flir.com/science/display/?id=44791>

TGA-DSC figure (slides 19-20): <http://www.tainstruments.com/wp-content/uploads/sdt.pdf>

Thank you. Questions?

Acknowledgement

This material is based upon work supported by the U.S. Department of Energy, National Nuclear Security Administration, under Award Number DE-NA0002375. The views and opinions of the authors expressed herein do not necessarily state or reflect those of the United States Government or any agency thereof.



Supplemental



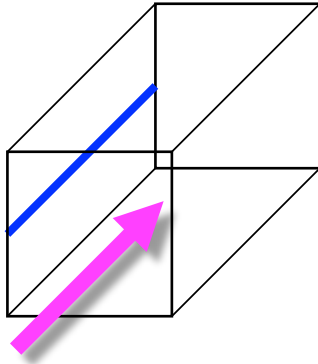
Other Institute Presentations

- Wednesday, June 8th
 - 70. “Heat Transfer and Temperature Behavior of a Maximum O₂ Concentration Oxy-Coal Flame”
 - 11:50 am – Oxyfuel Technologies I
 - 67. “Pilot-Scale Investigation and Modeling of Heat Flux and Radiation from an Oxy-coal Flame”
 - 4:00 pm – Oxyfuel Technologies II
 - 52. “Thermal Characterization of a 1.5 MW Pulverized-coal Furnace Using Infrared Heat Flux, Total Heat Flux and Measured Heat Loss”
 - 4:40 pm – Oxyfuel Technologies II
- Thursday, June 9th
 - 76. “Simulation and Validation of 15 Mwth Oxy-Coal Power Boiler”
 - 10:30 am – Oxyfuel Technologies III
 - 78. “Uncertainty Quantification for Coarse-Grained Modeling of Coal Devolatilization”
 - 11:10 am – Oxyfuel Technologies III
 - 79. “Towards Next Generation Simulations of Full-Scale Coal-Fired Boilers”
 - 11:30 am – Oxyfuel Technologies III

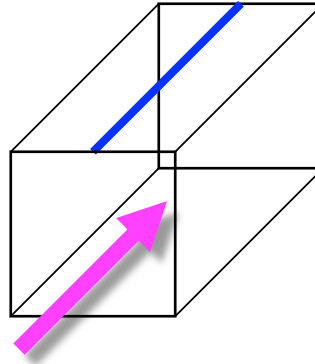
Extra Plots - Porosity

■ = sampling location ■ = flame

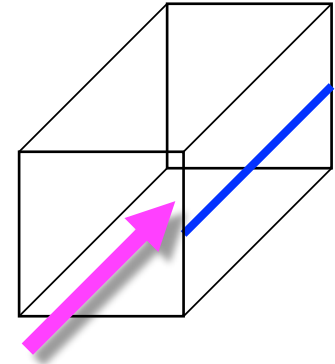
Left Wall



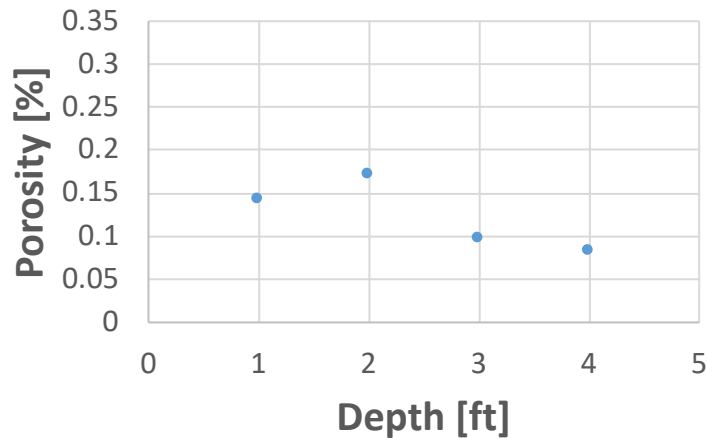
Ceiling



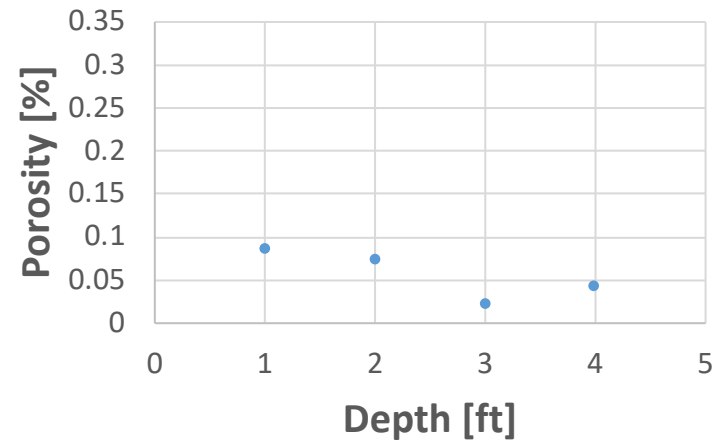
Right Wall



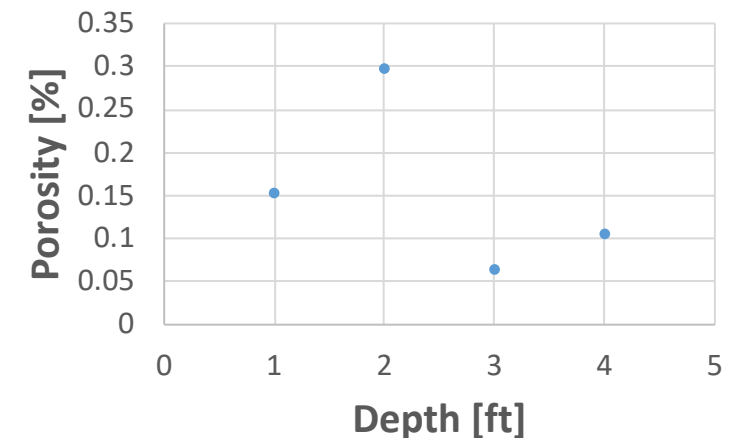
Left



Ceiling



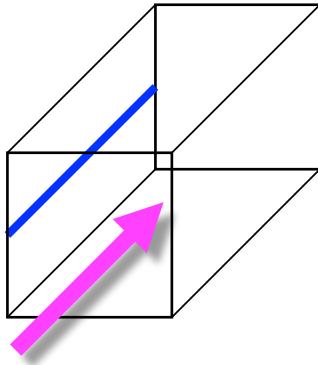
Right



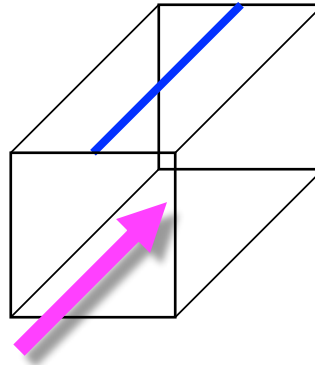
Extra Plots - Density

■ = sampling location ■ = flame

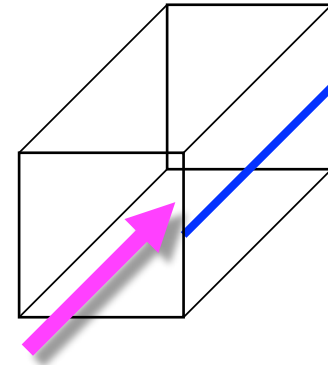
Left Wall



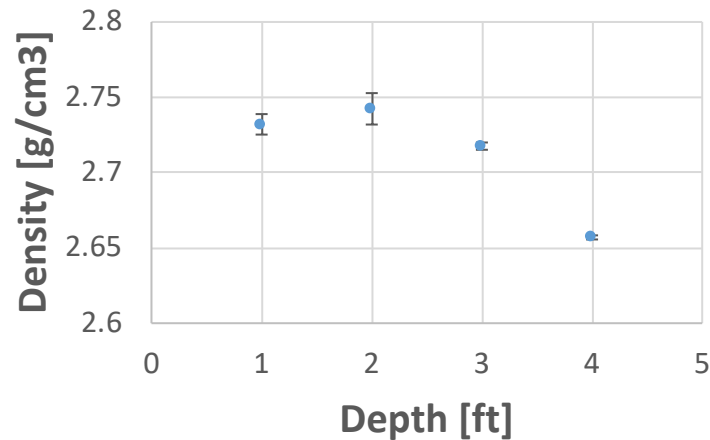
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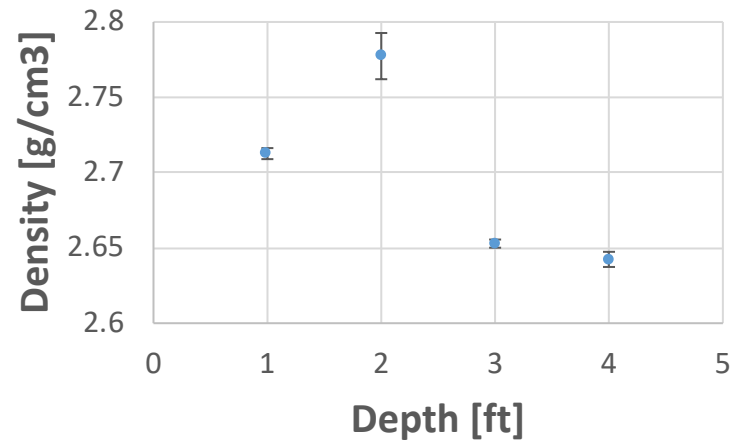
Right Wall



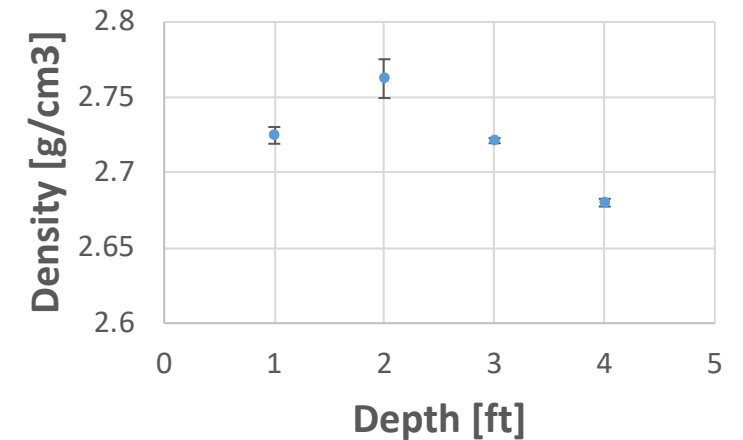
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Ceiling



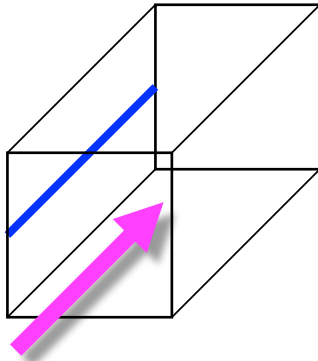
Right



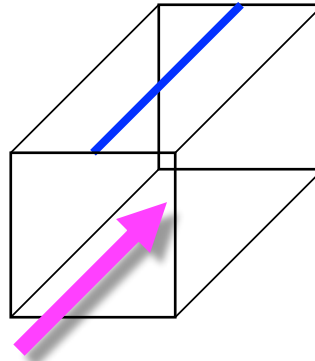
Extra Plots – Thermal Diff

■ = sampling location ■ = flame

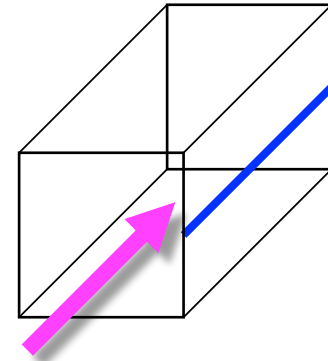
Left Wall



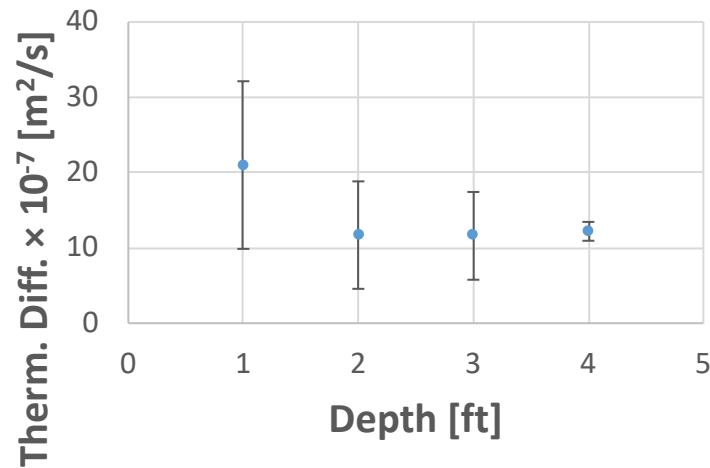
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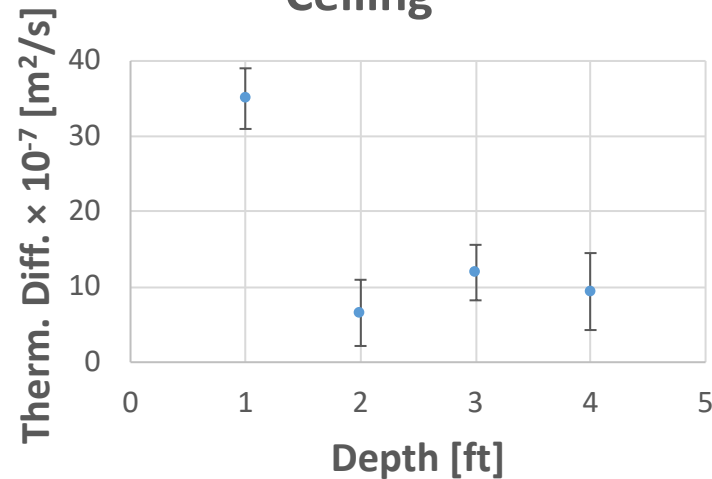
Right Wall



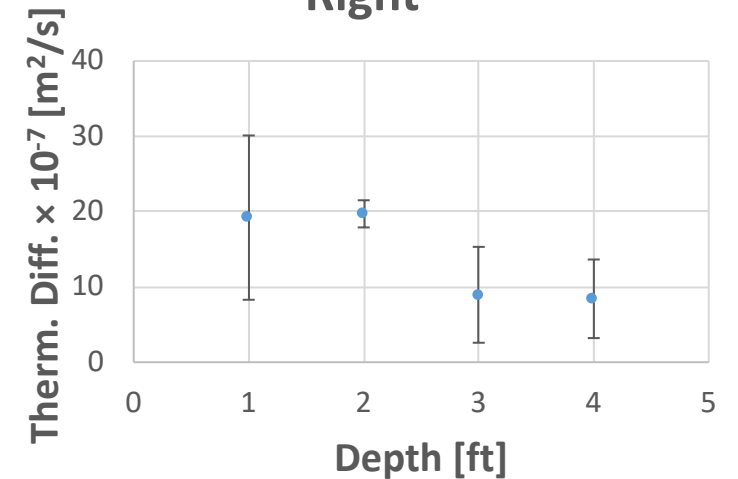
Left



Ceiling



Right

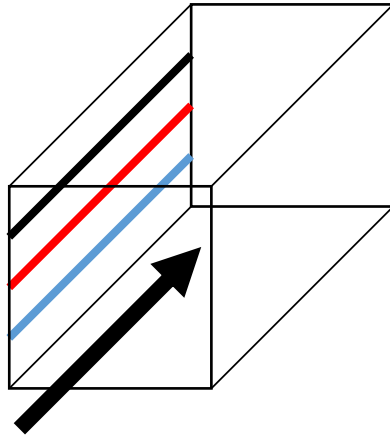


Emissivity

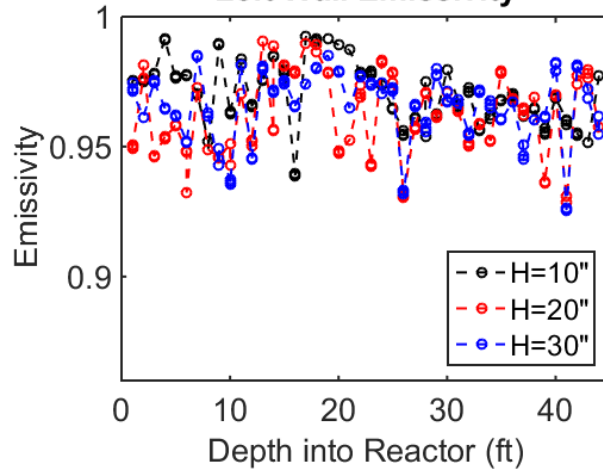
- Diffuse reflectance cell in FT/IR to measure complex refractive index, n_λ and k_λ , of the deposits at room temperature
- Spectral reflectivity:
 - $\rho_\lambda = \frac{(n_\lambda - 1)^2 + k_\lambda^2}{(n_\lambda + 1)^2 + k_\lambda^2}$
- Kirchhoff's law ($\varepsilon_\lambda = \alpha_\lambda$) and radiation balance:
 - $\varepsilon_\lambda + \rho_\lambda + \tau_\lambda = 1$
- Assuming opaque medium:
 - $\varepsilon_\lambda = 1 - \rho_\lambda$
- Total emissivity approximated:
 - $\varepsilon \approx \frac{\int_{2.5 \mu m}^{25 \mu m} \varepsilon_\lambda E_{b,\lambda}}{\int_{2.5 \mu m}^{25 \mu m} E_{b,\lambda}}$

Emissivity

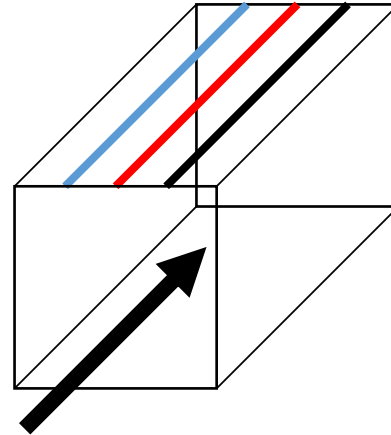
Left Wall



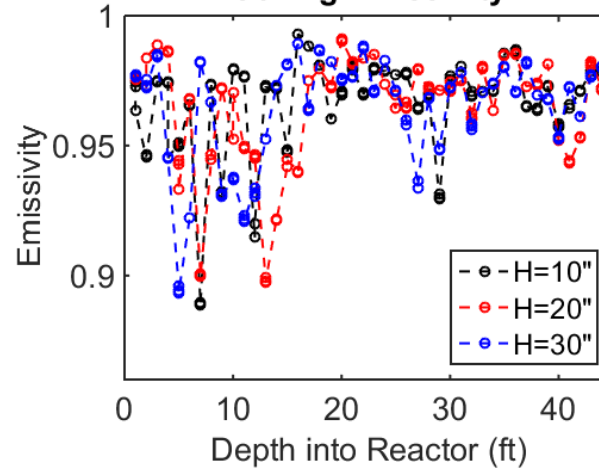
Left Wall Emissivity



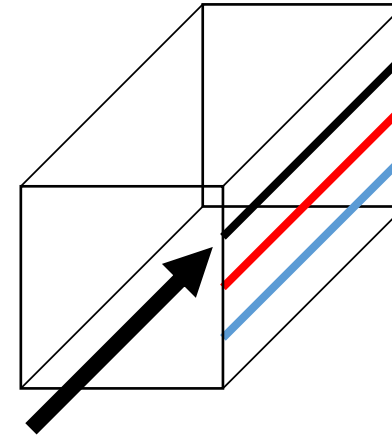
Ceiling



Ceiling Emissivity



Right Wall



Right Wall Emissivity

